

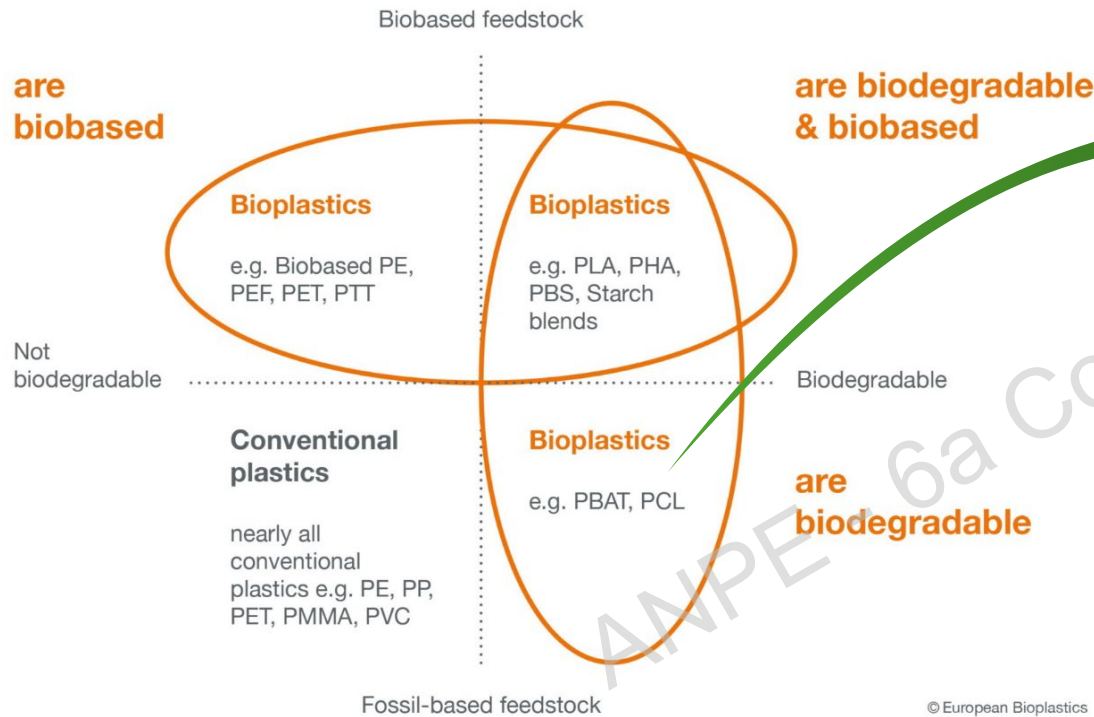
Valorization of biopolymers waste through chemical recycling

Supervisor: Prof. Michele Modesti

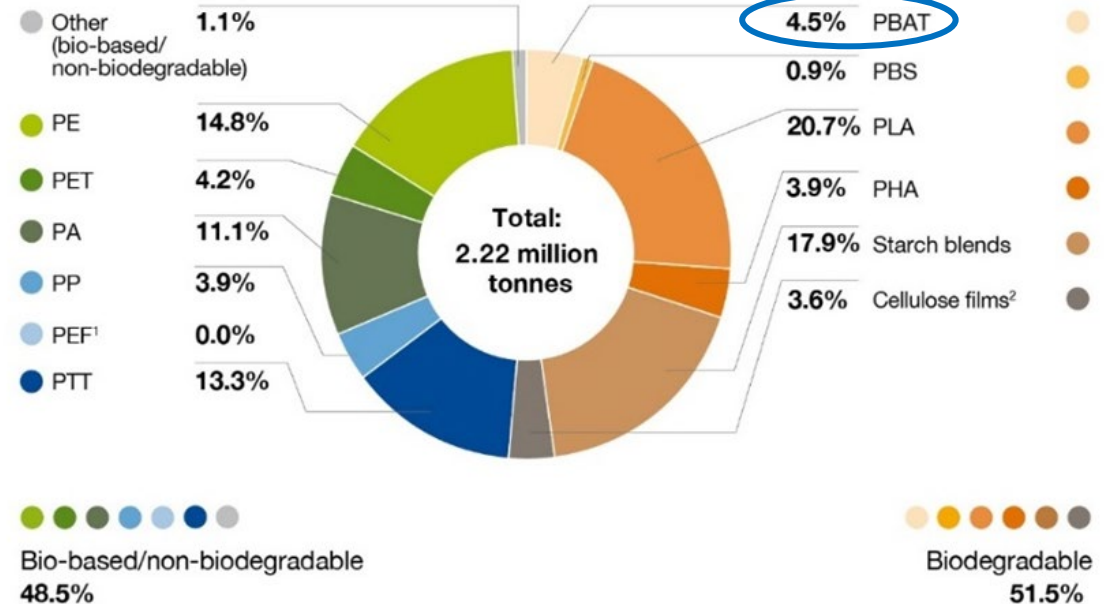
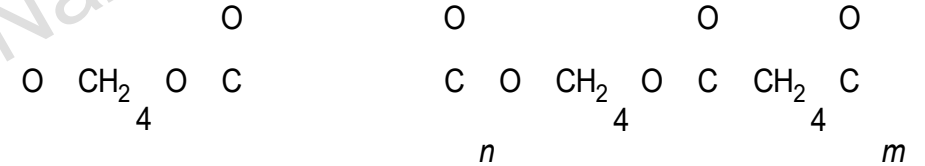
Assistant supervisor: Dr. Riccardo Donadini

6° Conferenza Nazionale Poliuretano Espanso rigido

Introduction to Biopolymers



Poly(butylene adipate terephthalate) (PBAT)

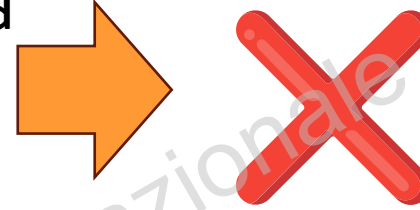


Introduction to End-of-Life Scenarios

Biodegradation as EoL scenario?

High times required

No recovering



CIRCULAR ECONOMY



This thesis

Mechanical recycling

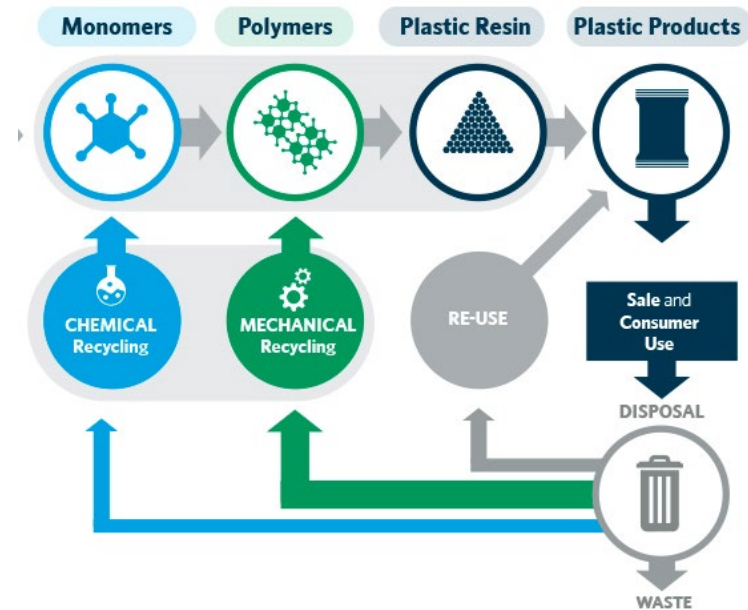
Chemical recycling

Thermo Recycling

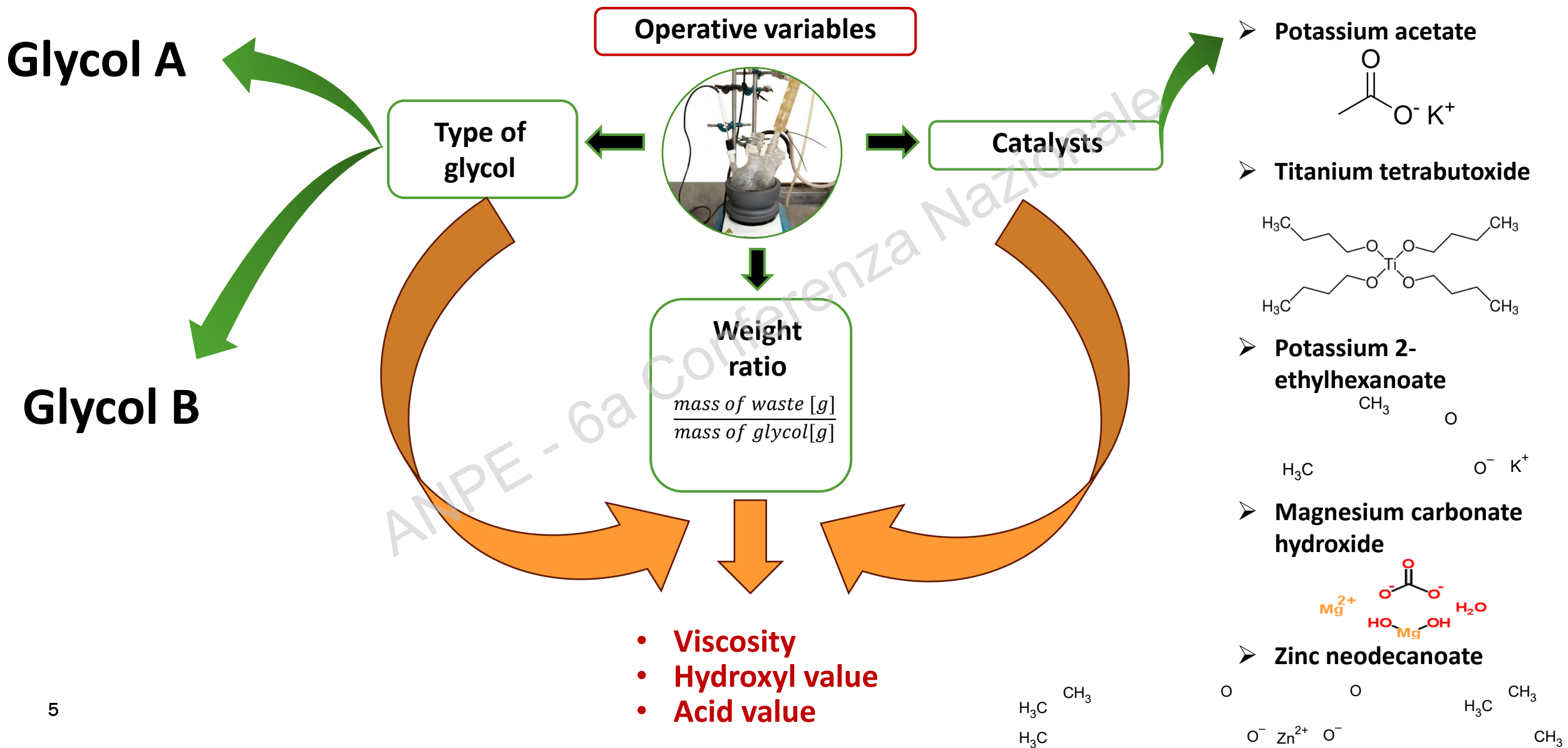
Recovers polymer

Recovers monomer

Recovers energy



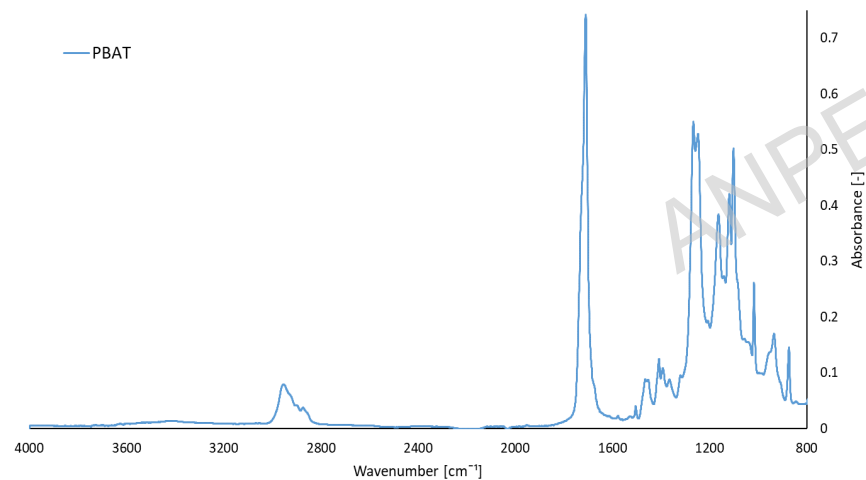
Objective of the thesis



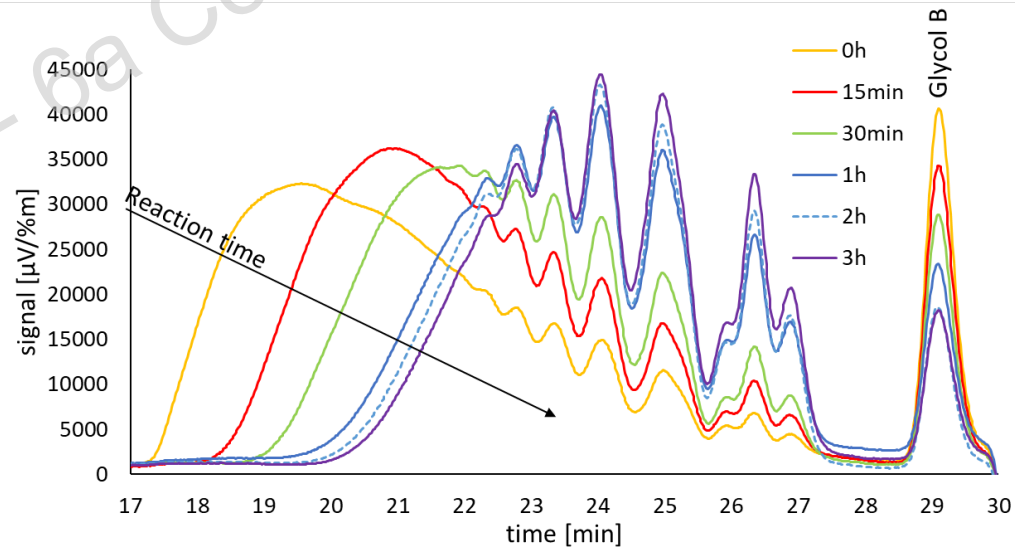
Characterization



Fourier-transform Infrared Spectroscopy (FTIR)



Gel Permeation chromatography (GPC)

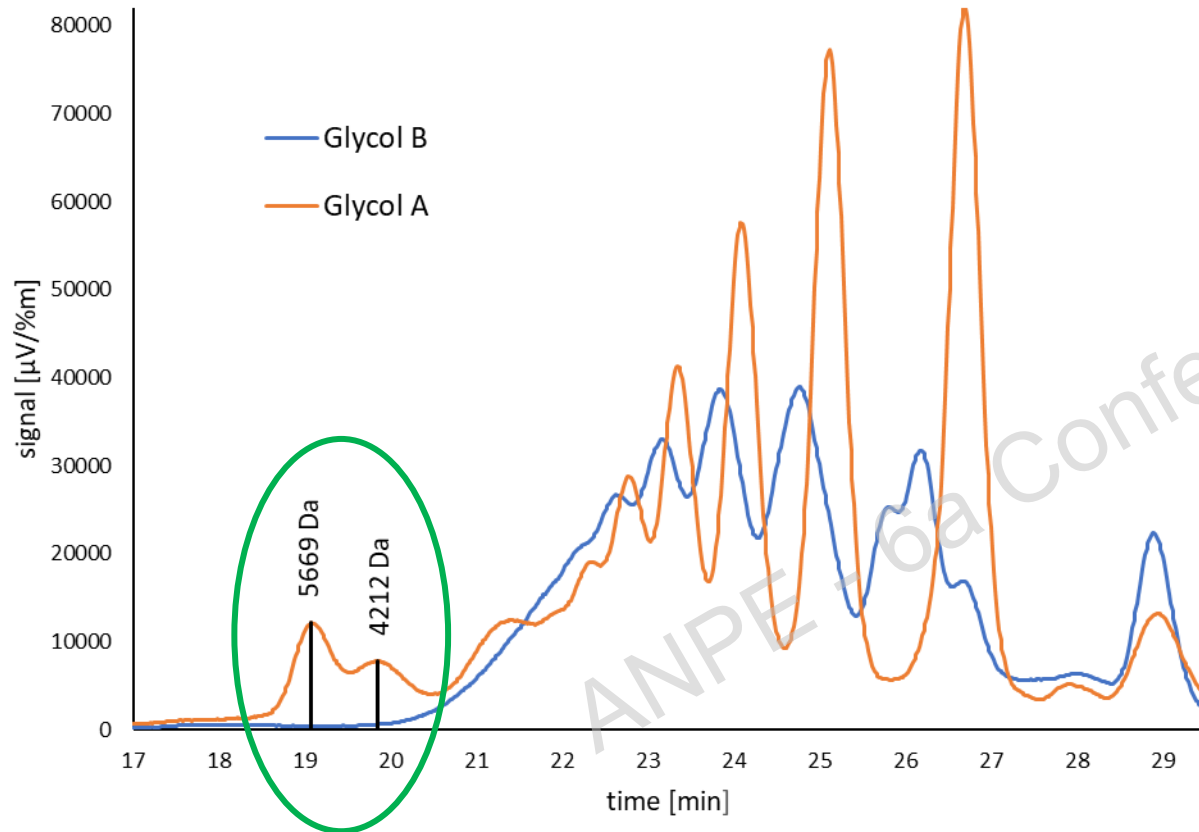


Dynamic viscosity



Titration for hydroxyl and acid values

Glycol A vs Glycol B



Fixed parameters

- ✓ Temperature
- ✓ Weight ratio
- ✓ Reaction time
- ✓ Catalyst
- ✓ Catalyst concentration

Glycol B is more reactive than Glycol A

Tests with Glycol A

Fixed parameters

- ✓ Weight ratio
- ✓ Reaction time

ID test	Viscosity [mPa·s]	HV [mg _{KOH} /g]	AV [mg _{KOH} /g]
TEST_1	3300	308	2.9
TEST_2	5750	257	8.3
TEST_3	3200	273	12
TEST_4	3200	296	20
TEST_5	5750	261	15

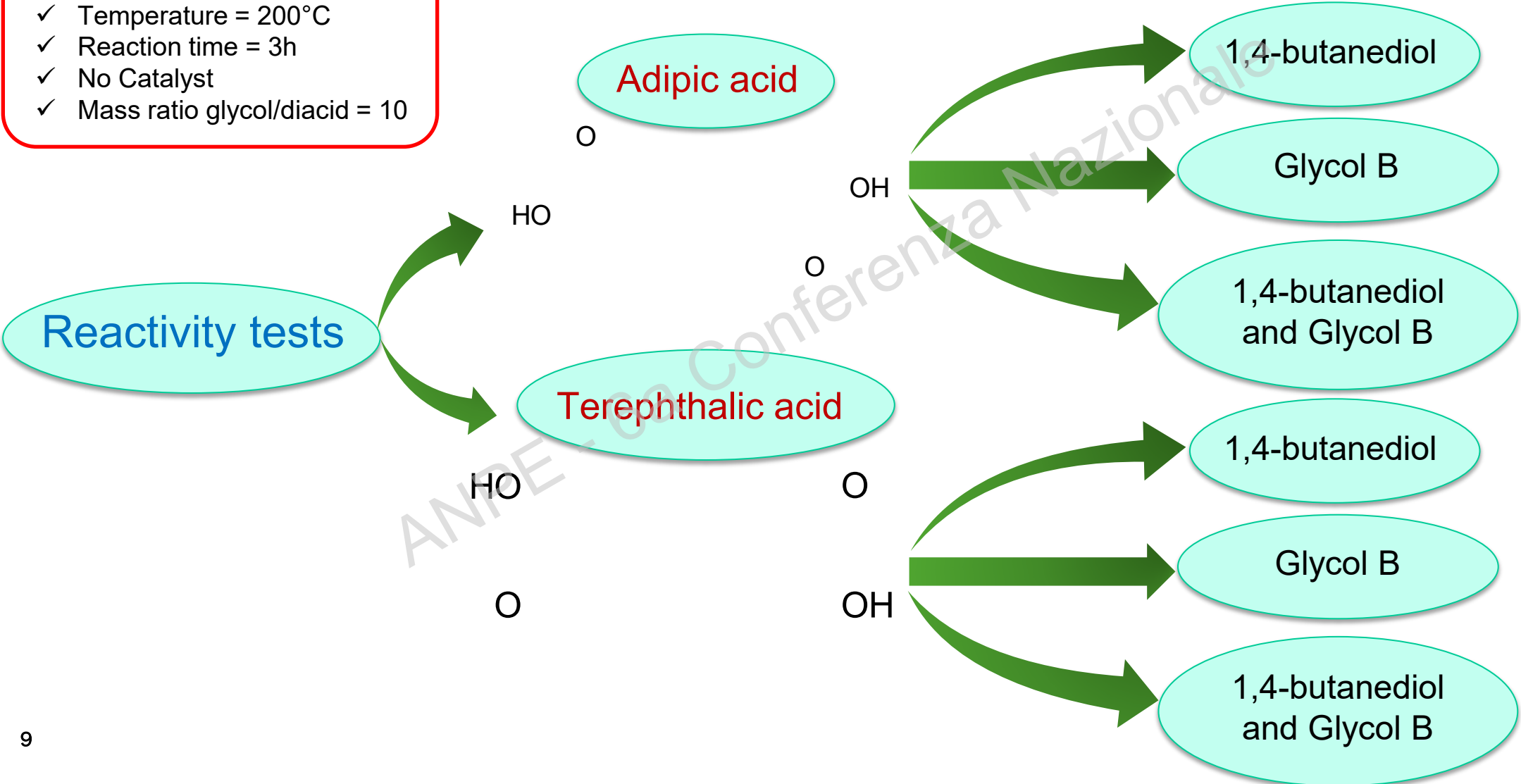
All between 200 and 500 mg_{KOH}/g

All below 8000 mPa·s

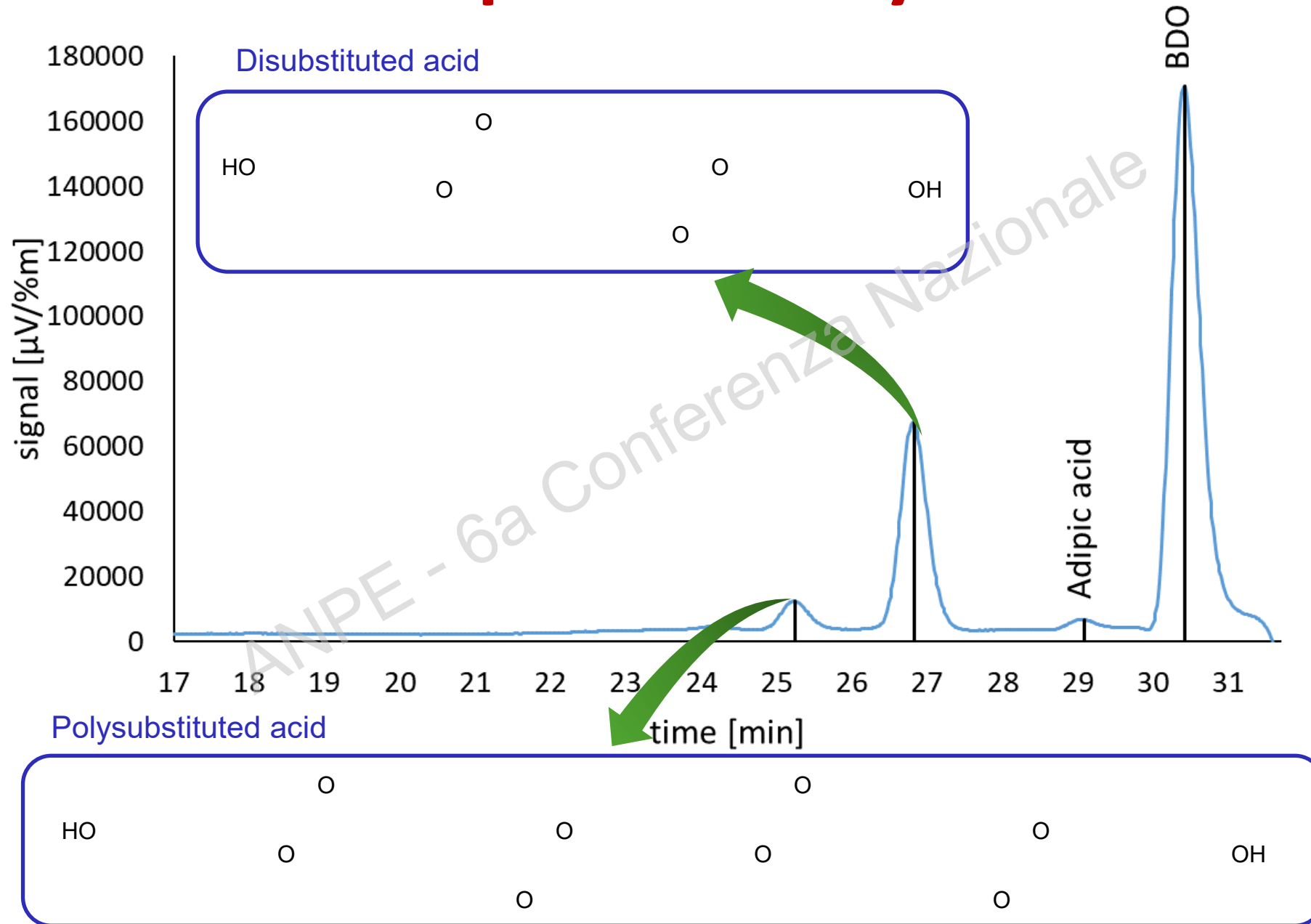
Lowest acid number

Reactivity tests

- Fixed parameters**
- ✓ Temperature = 200°C
 - ✓ Reaction time = 3h
 - ✓ No Catalyst
 - ✓ Mass ratio glycol/diacid = 10



Gpc reactivity tests



Kinetic of the tests with adipic acid

$$v = \frac{d[COOR]}{dt} = k[COOH][OH][H^+]$$



Rate of polycondensation without an external catalyst

$$[OH] \sim \text{constant}$$

$$[H^+] = K_a^{\frac{1}{2}}[COOH]^{\frac{1}{2}}$$



Weak acid equilibrium

$$[COOH] = [COOH]_0 - [COOR]$$

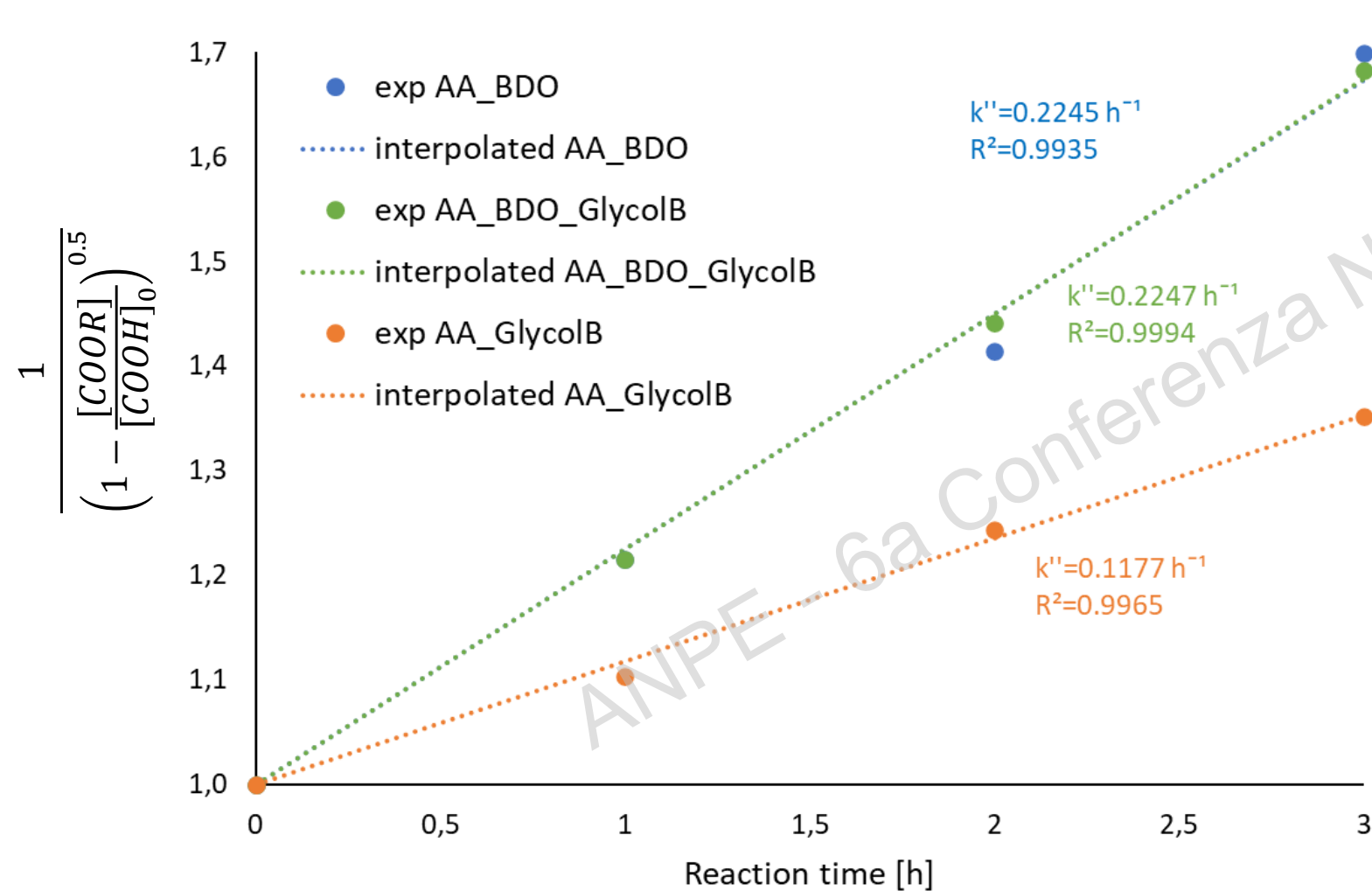
$$v = \frac{d[COOR]}{dt} = k'([COOH]_0 - [COOR])^{\frac{3}{2}}$$

$$\frac{1}{\left(1 - \frac{[COOR]}{[COOH]_0}\right)^{\frac{1}{2}}} = k''t + 1$$

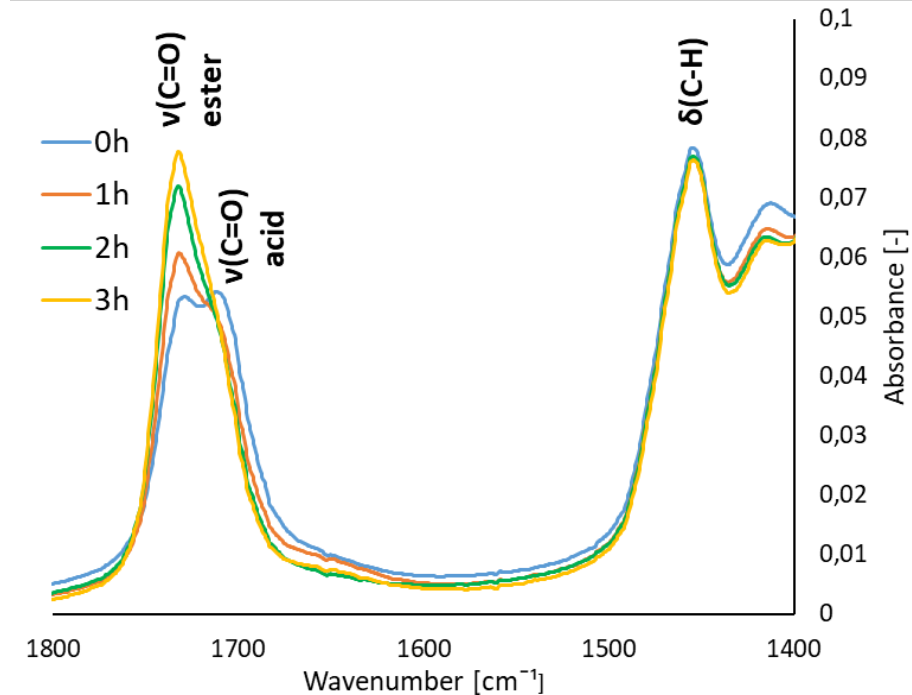


Final expression after integration

Kinetic of the tests with adipic acid



$$\frac{1}{\left(1 - \frac{[COOR]}{[COOH]_0}\right)^{\frac{1}{2}}} = k''t + 1$$

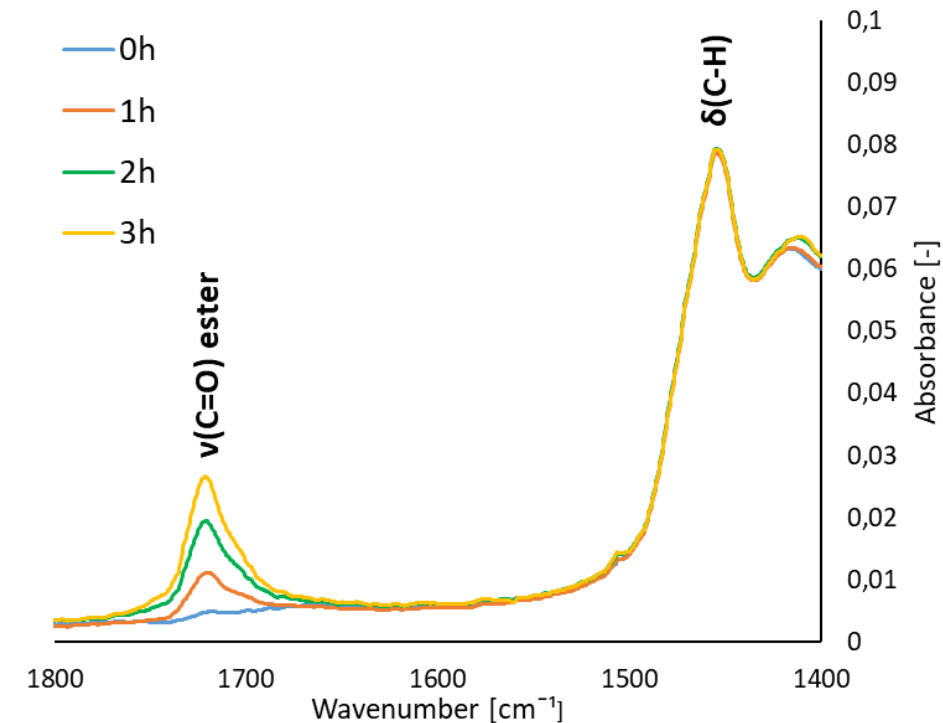
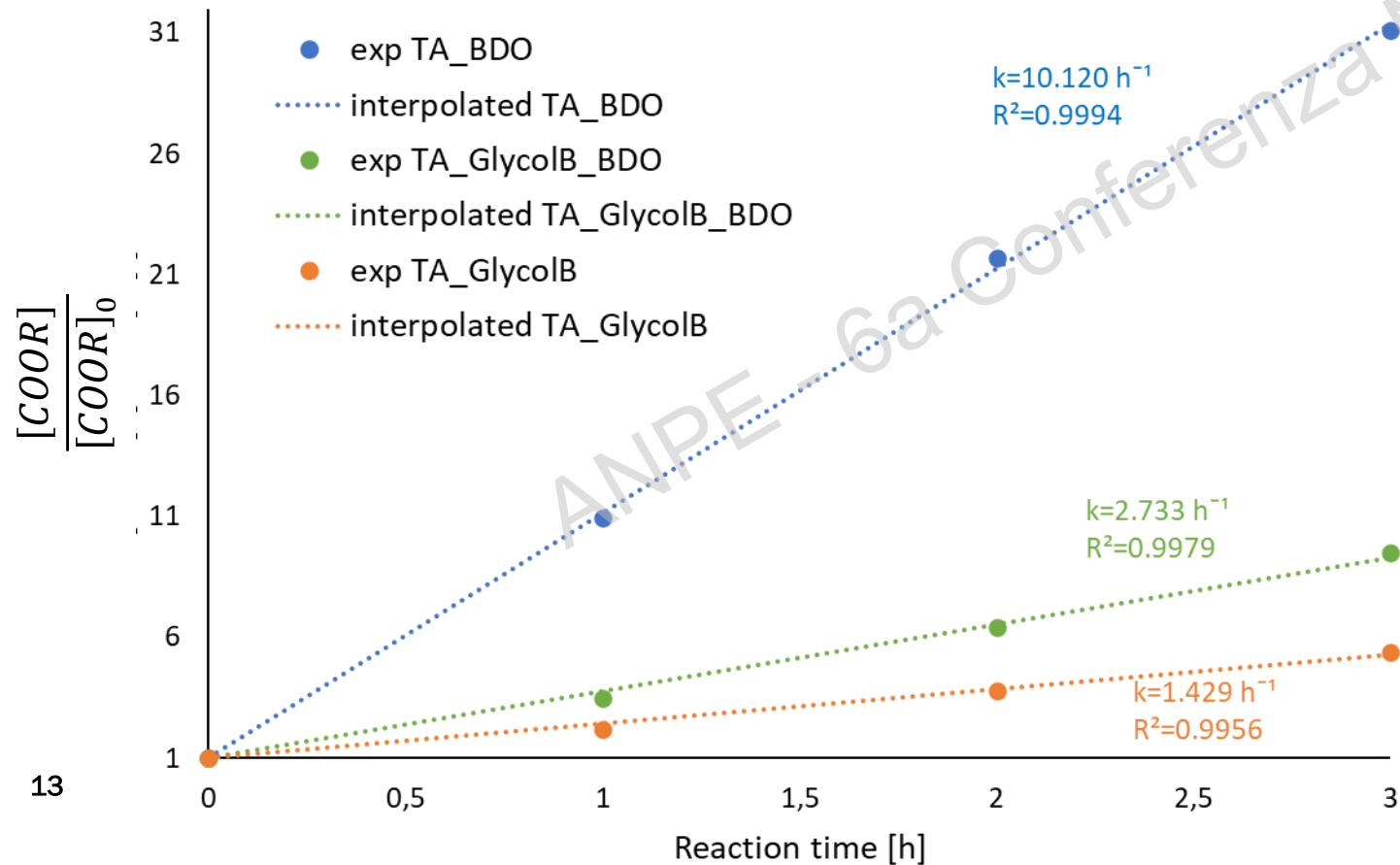


Kinetic of the tests with terephthalic acid

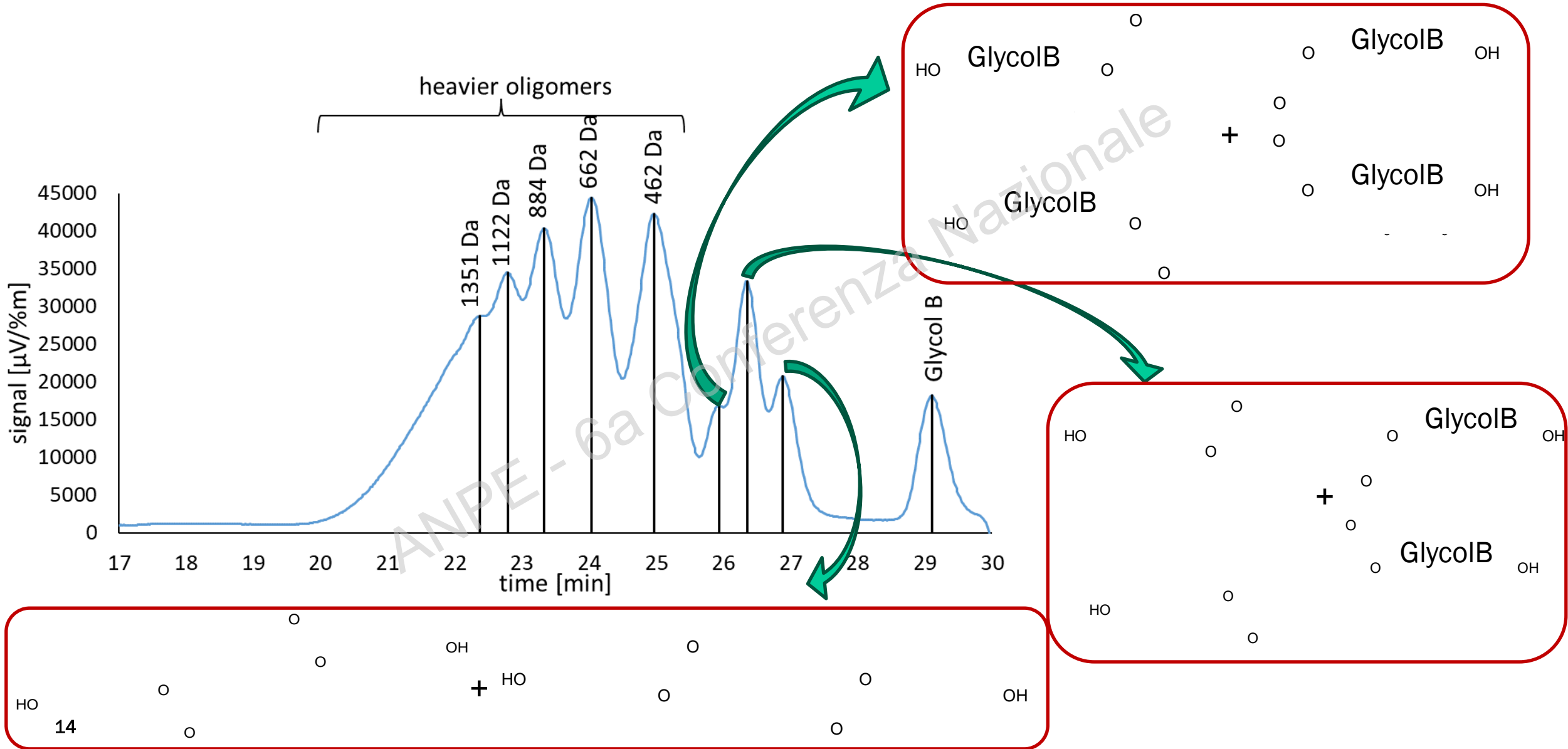
Low solubility of the acid

Mass transfer from solid to liquid is the controlling step

$$\frac{[COOR]}{[COOR]_0} = k \cdot t + 1$$



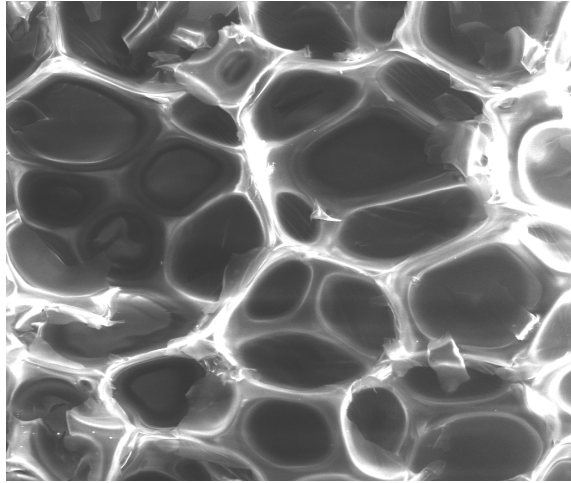
Gpc glycolyzate used for foams



Foam formulation

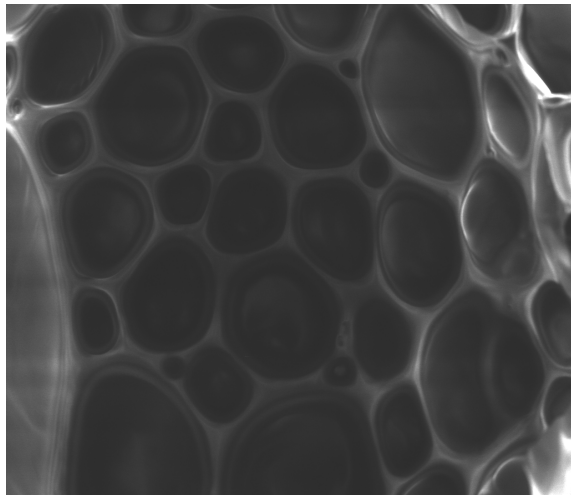
	Component	REF	25% RP	50% RP	75% RP	100% RP
Industrial polyols	Pol 1 [g]	50	25	-	-	-
	Pol 2 [g]	50	50	50	25	-
Glycolyzate	RP [g]	-	25	50	75	100
Catalysts	Cat 1 [g]	0.86	1	1.2	1.2	1.3
	Cat 2 [g]	3	3	3	2.7	3
Silicone	B8443 [g]	2	2	2	2	2
Blowing agents	H ₂ O [g]	1	1	1	1	1
	C ₅ [g]	10.2	11.6	11.2	10.8	11.3
Isocyanate	MDI [g]	217	210	203	213	223
Characteristic times	Cream [s]	29	27	16	20	27
	Gel [s]	48	56	43	56	69
	Tack-free [s]	59	80	70	85	112

Pur/pir Foams

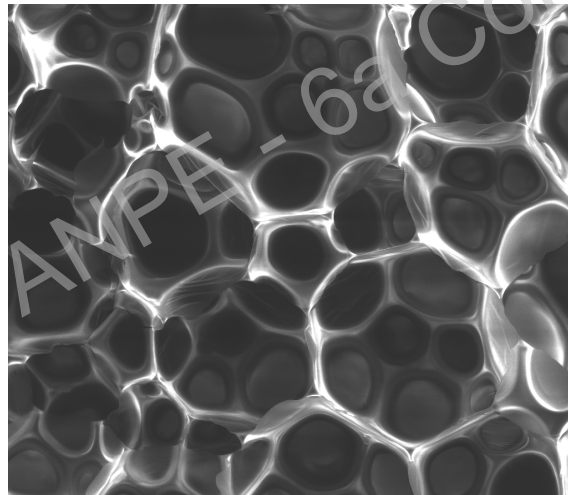


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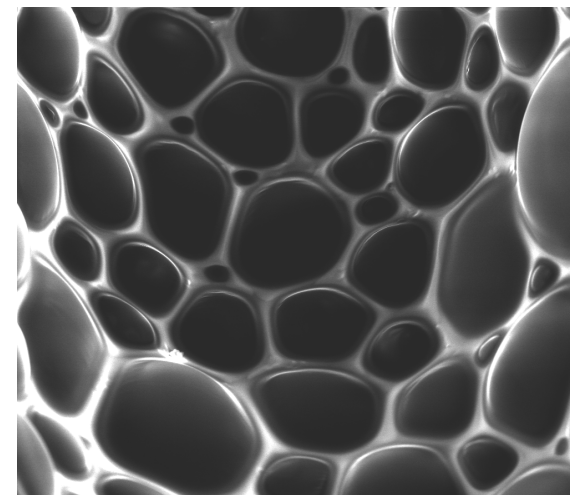
	ρ [kg/m ³]	$\sigma_{//,norm}$ [kPa]	$\sigma_{\perp,norm}$ [kPa]	Aniso ratio [-]	λ [mW/(m·K)]	d [μ m]
REF	40.4	318±5	141±4	2.25	25.0±0.2	136±23
25% RP	42.9	349±23	160±11	2.18	25.2±0.2	114±18
50% PBAT	42.3	360±26	179±10	2.01	24.2±0.2	103±19
75% PBAT	42.8	353±7	165±13	2.14	23.7±0.2	98±20
100% PBAT	43.6	305±6	167±14	1.83	24.6±0.2	167±31



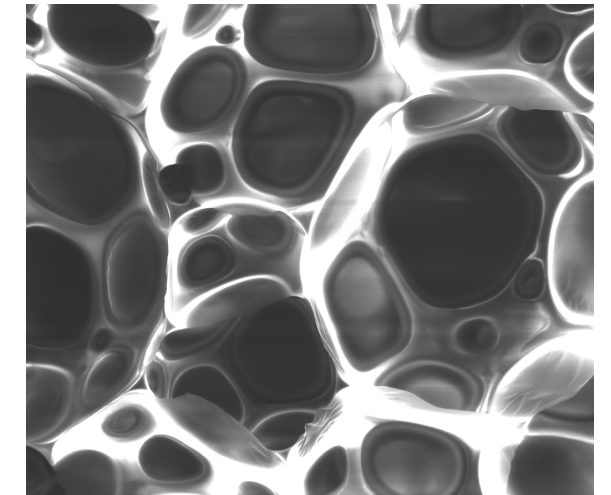
25% PBAT



50% PBAT



75% PBAT



100% PBAT

Conclusions and further studies

- **Glycolysis** is a **promising** method for recycling PBAT;
- PUR/PIR foams can be produced with up to **100% of glycolyzate** with **comparable performances** with respect to reference foam;
- Since **PBAT** is mainly utilized in **blends** with other polymers, additional research will be done.

*Thank you for
your attention*

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